

Hydrogen will play an important role in the decarbonisation of sectors that cannot rely exclusively in electrification (e.g. transportation, energy and carbon intensive industries) [1]. However, hydrogen economies will require a reformation and expansion of the current gas transportation and storage infrastructure, to accommodate high volumes of pure or blended hydrogen.



**Pipelines** are a crucial element of that infrastructure, which are particularly susceptible to *hydrogen induced failure* (HIF), an unpredictable phenomena that often leads to substantial economic losses and environmental damages.

Table 1: Chemical composition and mechanical properties of X65 pipeline steel.  $\sigma_{v0.2}$  – Offset

Figure 1: Roadmap of South Wales Industrial Cluster (SWIC) project [2].

#### yield strength at 0.2%, UTS – Ultimate Tensile Strength Mass fraction (%), max. value **Mechanical properties** Fracture **Elongation at** σ<sub>y0.2</sub> (MPa) UTS (MPa) С Ρ S Orientation strength Mn Si fracture (%) (MPa) 261 ± 5 502 ± 6 574 ± 9 $32.0 \pm 0.3$ Longitudinal 0.003 0.075 0.02 0.225 1.55 $513 \pm 0.5$ 580 ± 8 $33.5 \pm 0.3$ 266 ± 2

Transverse

## High Frequency Induction (HFI) welded pipelines



Grade: API 5L X65

Diameter: 508 mm

Thickness: 15.9 mm



## Factors that lead to pipeline failure:

- Higher strength
- Elevated internal pressure
- Cyclic stresses
- Corrosion









Figure 2: Optical microscope images of X65 microstructure (a) weld and HAZ cross-section (d) base material Microstructure composed of ferrite matrix (grey) with pearlite (black).

# **INTERACTION OF HYDROGEN WITH METALS**

Hydrogen transport into a certain critical location can be described by the following reaction steps [3, 4]:

#### **Reaction 1**

Gas – phase diffusion of molecular hydrogen  $(H_2)$  to the crack surface

#### **Reaction 2**

H<sub>2</sub> dissociation at metal surface and physical adsorption of atoms

#### **Reaction 3**

Adsorbed atoms migrate across the metal surface and consequent chemisorption

#### **Reaction 4**

 $r_1 = k_1 P$ rate constant

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P - H_2 pressure
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r_2 = k_2 P^{\overline{2}} (1 - \theta)
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 $\theta$  - H surface coverage

 $r_3 = k_3 grad u$ 

grad u – gradient in surface hydrogen concentration

$$k = k_{\Lambda} \theta \left[ 1 - \left( \frac{u}{u} \right) \right]$$

## HYDROGEN PERMEATION TESTING (ISO 17081:2014)<sup>[5]</sup>



## Adsorbed atoms dissolve into the

metal

### **Reaction 5**

Atoms diffuse to the critical location, causing embrittlement



u – hydrogen concentration just inside the metal surface  $u_s$  – saturation concentration of hydrogen in the metal

 $r_5 = D\left(u - \frac{u_l}{l}\right)$ 

D – diffusion coefficient

Different cathodic charging conditions

- Galvanostatic charging (fixed current), creates a flux of H towards the surface
- Potentiostatic charging potential), (fixed promotes the concentration of H at the surface

 $u_l$  – hydrogen concentration at the critical location at l distance from the metal surface

The overall transport reaction will be the sum of the individual reactions and can involve reactions occurring in opposite directions, consecutively and in parallel. If any of the reaction steps is hindered or eliminated, the structure will be less susceptible to embrittlement.

## REFERENCES

[1] N. P. Brandon and Z. Kurban, Phil. Trans R. Soc. A, 375:20160400 (2017), 31. [2] https://www.swic.cymru/ (accessed on 10/02/2021) [3] ASTM STP 543: Hydrogen Embrittlement Testing, ASTM, 1972 [4] J. Toribio and V. Kharin, Nuclear Engineering and Design 182 (1998) 149-163 [5] S. Papavinasam, Corrosion Control in the Oil and Gas Industry, Gulf Professional Publishing (2014) [7] A. Griesche et al., *Phys. Procedia*, **69** (2015).





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